## **Supplementary Materials**

Multiphysics simulation details including initial conditions, boundary conditions, and simulation parameters are arranged in this supplementary data. **Table S1** summarizes the initial and boundary conditions applied in  $UV/H_2O_2$  simulation. Parameters used in this simulation are listed in **Table S2**. To improve understanding, visualized simulation domains and boundaries of the  $UV/H_2O_2$  reactor are shown in **Fig. S1**.

Table S1. Initial and boundary conditions for multiphysics simulations

 $-\mathbf{n}\cdot(-D_{\mathrm{P}1}\nabla G)=-\mathrm{q}_{\mathrm{r,net}},\,\mathrm{q}_{\mathrm{r,net}}=\frac{1}{2}(4\pi I_{\mathrm{b,w}}-G)\,(\mathrm{black\;wall})$ 

 $I_i = I_{\text{wall}}$ 

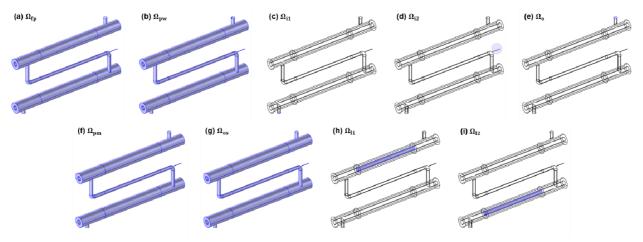
Initial conditions			
Equations	Location		
$\mathbf{u}_x = 0,  \mathbf{u}_y = 0,  \mathbf{u}_z = 0,  p = 0$	at $\Omega_{ m fp}$		
$c = c_{0,i}$	at $\Omega_{ m fp}$		
$\mathit{GG}_{i}$ (The blackbody radiative intensity at initial temperature)	at $\Omega_{ m pm}$		
Boundary conditions			
Equations	Location		
$\mathbf{u} \cdot \mathbf{n} = 0 \text{ (No slip)}$	at $\Omega_{ m pw}$		
$\mathbf{u} = -U_0 \mathbf{n}$ (Normal inflow velocity), $\mathbf{n} \cdot (\mathbf{J}_i + \mathbf{u} \mathbf{c}_i) = \mathbf{n} \cdot (\mathbf{u} \mathbf{c}_{\text{in},i})$	at $\Omega_{i1}$ and $\Omega_{i2}$		
$[-nI + K]n = -n^{\wedge}_{0}n$ , $n^{\wedge}_{0} < n_{0}$ , $\forall k \cdot n = 0$ , $\forall \epsilon \cdot n = 0$ , $\mathbf{n} \cdot D_{i} \forall c_{i} = 0$	at $\Omega_{\circ}$		

at  $\Omega_{os}$ 

at  $\Omega_{l1}$  and  $\Omega_{l2}$ 

Table S2. Simulation parameters for multiphysics simulations (a: assumed, c: controlled, m: measured)

Description	Symbol	Value	Ref.
Temperature [K]	T	298.15	a
Fully developed inflow flow rate [L/min]	$U_0$	7	С
Density of liquid water [kg/m³]	p	1000	a
Viscosity of liquid water [Pa·s]	$\mu$	0.001	a
Absorption coefficient [1/cm]	$\kappa$	0.05	a
Scattering coefficient [1/cm]	$\sigma_{_{S}}$	0.003	a
Boundary radiation intensity [W/(cm <sup>2</sup> ×sr)]	$I_{\mathbf{wall}}$	1500	a
Initial concentration of H <sub>2</sub> O <sub>2</sub> [mg/L]	$c_{0,H2O2}$	15, 10, 7.5, 5, 2.5	С
Initial concentration of CO <sub>3</sub> [mol/L]	c <sub>0,CO3</sub>	$1 \times 10^{-16}$	a
Initial concentration of CO <sub>3</sub> <sup>2-</sup> [mol/L]	c <sub>0,CO32</sub> -	$2.91 \times 10^{-7}$	a
Initial concentration of caffeine [mol/L]	$c_{0,caffeine}$	$1 \times 10^{-5}$	С
Initial concentration of DOC [mg/L]	$c_{0,DOC}$	4.5	m
Initial concentration of H <sup>+</sup> [mol/L]	$c_{0,H}$	$1 \times 10^{-7}$	m
Initial concentration of H <sub>2</sub> CO <sub>3</sub> [mol/L]	c <sub>0,H2CO3</sub>	$1.119 \times 10^{-4}$	m
Initial concentration of HCO <sub>3</sub> - [mol/L]	$c_{0,HCO3-}$	$5.81 \times 10^{-4}$	a
Initial concentration of O <sub>2</sub> [mol/L]	$c_{0,O2}$	$2.656 \times 10^{-4}$	m
Initial concentration of OH [mol/L]	$c_{0,OH-}$	$1 \times 10^{-7}$	m
Initial concentration of $pCBA$ [mol/L]	$c_{0,pCBA}$	$1 \times 10^{-5}$	C
Inlet concentration of H <sub>2</sub> O <sub>2</sub> [mg/L]	$c_{\mathrm{in},H2O2}$	15, 10, 7.5, 5, 2.5	С
Inlet concentration of CO <sub>3</sub> [mol/L]	$c_{\mathrm{in}{\it CO3}\cdot-}$	$1 \times 10^{-16}$	a
Inlet concentration of CO <sub>3</sub> <sup>2-</sup> [mol/L]	$c_{\mathrm{in}co32-}$	$2.91 \times 10^{-7}$	a
Inlet concentration of caffeine [mol/L]	$c_{\mathrm{in},caffeine}$	$1 \times 10^{-5}$	C
Inlet concentration of DOC [mg/L]	$c_{\mathrm{in},DOC}$	4.5	m
Inlet concentration of H <sup>+</sup> [mol/L]	$\mathrm{c}_{\mathrm{in},H}$	$1 \times 10^{-7}$	m
Inlet concentration of H <sub>2</sub> CO <sub>3</sub> [mol/L]	$c_{\mathrm{in},H2CO3}$	$1.119 \times 10^{-4}$	m
Inlet concentration of HCO <sub>3</sub> [mol/L]	$c_{\mathrm{in},HCO3-}$	$5.81 \times 10^{-4}$	a
Inlet concentration of O <sub>2</sub> [mol/L]	$c_{\mathrm{in},o_2}$	$2.656 \times 10^{-4}$	m
Inlet concentration of OH <sup>-</sup> [mol/L]	$c_{\mathrm{in},OH-}$	$1 \times 10^{-7}$	m
Inlet concentration of $pCBA$ [mol/L]	$c_{\mathrm{in},p\mathit{CBA}}$	$1 \times 10^{-5}$	C
Diffusivity of all chemical species [m <sup>2</sup> /s]	D	1 × 10 <sup>-9</sup>	a



(a)~(e): CFD and transport, (f)~(i): radiation

Fig. S1. Visualization of simulation domain and boundary of the UV/H<sub>2</sub>O<sub>2</sub> reactor. The corresponding part is shown in purple: (a) flow path domain ( $\Omega_{fp}$ ) is the domain for the CFD and transport simulation. (b) pipe wall ( $\Omega_{pw}$ ), (c) inlet 1 ( $\Omega_{11}$ ), (d) inlet 2 ( $\Omega_{12}$ ), and (e) outlet ( $\Omega_{o}$ ) are the boundaries for the CFD and transport simulation. (f) participating medium ( $\Omega_{pm}$ ) is the domain for the radiation simulation. (g) opaque surface ( $\Omega_{os}$ ), (h) lamp 1 ( $\Omega_{11}$ ), and (i) lamp 2 ( $\Omega_{12}$ ) are the boundaries for the radiation simulation.

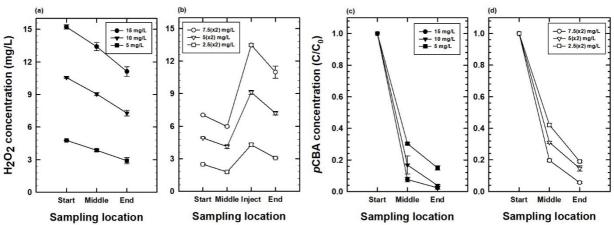


Fig. S2.  $H_2O_2$  concentration change for (a) single injection and (b) two-step injection  $UV/H_2O_2$  experiments. pCBA concentration change for (c) single injection and (d) two-step injection  $UV/H_2O_2$  experiments ( $[pCBA]_0 = 10$  uM).

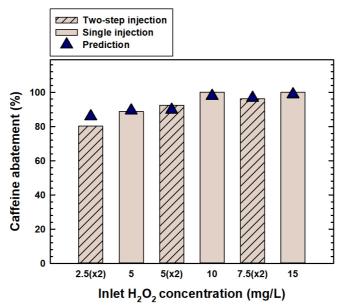


Fig. S3. Experimental results vs. prediction values of caffeine abatement using pCBA degradation results and subsequent 'OH exposure calculations ([caffeine]<sub>0</sub> = 10  $\mu$ M).